California Polytechnic State University, Pomona Aerospace Engineering Department Course: ARO 4180-01 Computational Fluid Dynamics

Lid-Driven Cavity Problem: Incompressible, Viscous, Rotational Flow

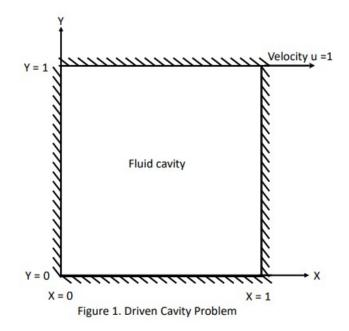
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#### **Problem Statement**



A figure of the Lid-Driven Cavity problem is shown above. A square cavity of sidelength equal to 1 has walls at locations x = 0, x = 1, y = 0, and y = 1. Its lid is located at the y = 1 wall that is moving to the right with a velocity of u = 1. Fluid inside the cavity is subject to incompressible, viscous, and rotational flow. Consider fluid with Reynold's Numbers of 10, 100, and 400, and iteratively solve an  $n \ge n$  grid for n equal to 8, 16, and 32. Using the Alternating Direction Implicit (ADI) Method solve the parabolic vorticity transport equation, and using the Point Successive Over Relaxation (PSOR) Method solve the elliptic stream function equation.

CFD Final Project Lid-Driven Carity Problem Nomenclature u-U, V=0 Top Wall: TW- (x,1) Botton Will: BW-(X.0) Lafe Wall: LW - (0,4) Right Will: RW-CLY Velocity field to = ui + Governing Equations (VITE Vorticity Transport Equation  $\frac{\partial 5}{\partial t} + u \frac{\partial 5}{\partial x} + v \frac{\partial 5}{\partial y} = \frac{1}{Re} \left( \frac{\partial^2 5}{\partial x^2} + \frac{\partial^2 5}{\partial y^2} \right)$ Steidy - State: u 25 + v 25 = 1 (25 + 225 Stream Function Equation (SFE) E = Dr. - Du  $v = -\frac{\partial \varphi}{\partial x} \cdot \xi$ , where  $\frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} = -5$ or EHIPHIL.

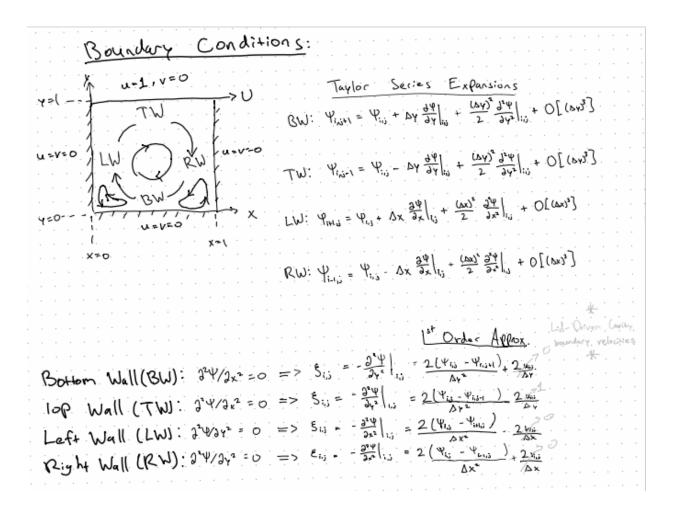
Sequential Solution Procedure 1.) Initialize 5 & 4 @ t=0 given û @ t=0 or make an initial guess Las for 3-0 problems) 2.) Solve VTE @ each interior grid point for t= (n+1) so L> obtain values of 5 using ADI method 3.) Solve SFE @ each interior grid point using 5 obtained in stel 2) using psor method 4) Find  $u = \frac{\partial \Psi}{\partial v} \in V = -\frac{\partial \Psi}{\partial x}$ 5.) Determine 5 on boundaries using 9 & 5 values at interior points. 6.) Check for convergence If not return to step 2 Matlab Implementation While error & ERROR-TOL . I. solve Vorticity transfort by ADI 1. X-Sweel 1. X-Sweel Solve Stream Function by PSOR solver for velocity fields using central differencia. 1- 4- dy => U13 = 41,1+1-41,1-1 . . d. T . . . 4:+(,i-4:-1,i 2× 2×

Finite-Difference Derivation

First Solve the Vorticity Transport Ego by ADI
$u \frac{\partial S}{\partial x} + v \frac{\partial S}{\partial y} = \frac{1}{R_e} \left( \frac{\partial S}{\partial x^2} + \frac{\partial^2 S}{\partial y^2} \right) (8-94)$
AOI Formulation: (8.8.1 p. 340)
$A_x S_{i_{1}i_{3}}^{n_1 t_1} + B_x S_{i_{1}i_{3}}^{n_1 t_1} + C_x S_{m_1}^{n_1 t_1} = D_x (8-101)$
Ay Singer + By Singer + (y Singer = Dy (8-102)
where $A_x = -\frac{1}{2}(\frac{1}{2}c_x + d_x)$ $A_y = -\frac{1}{2}(\frac{1}{2}c_y + d_y)$
$13_x = 1 + d_x \qquad 13_y = 1 + d_y$
$C_{x} = \frac{1}{2}(\frac{1}{2}c_{x} - d_{x})$ $C_{y} = \frac{1}{2}(\frac{1}{2}c_{y} - d_{y})$
and $D_{x} = \frac{1}{2} \left( \frac{1}{2} (y + dy) \xi_{i_{y+1}}^{n} + (1 - dy) \xi_{i_{y}}^{n} + \frac{1}{2} \left( -\frac{1}{2} (y + dy) \xi_{i_{y+1}}^{n} \right)$
$D_{y} = \frac{1}{2} \left( \frac{1}{2} (x + dx) \xi_{i+1,j}^{n+\frac{1}{2}} + (1 - dx) \xi_{i,j}^{n+\frac{1}{2}} + \frac{1}{2} \left( -\frac{1}{2} (x + dx) \xi_{i+1,j}^{n+\frac{1}{2}} \right) \right)$
Where
$L_x = u \frac{\Delta t}{\Delta x}$ , $L_y = v \frac{\Delta t}{\Delta y}$
$d_x = \frac{1}{Re} \frac{\Delta t}{(\Delta x)^2} d_y = \frac{1}{Re} \frac{\Delta t}{(\Delta y)^2}$

Solve Stream Function By PSOR  $\frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial x^2} = -5$ Point Successive Over - Relaxation Formulation Ψ K+1 = (1-ω)Ψ<sup>K</sup> + <u>W</u> 2 (1+β2) [ S<sup>a+1</sup><sub>10</sub> (D×)<sup>2</sup> + Ψ<sup>K</sup><sub>141</sub> + Ψ<sup>K+1</sup><sub>1-1</sub> + B<sup>2</sup>(Ψ<sup>K</sup><sub>10</sub> + Ψ<sup>K+1</sup><sub>10</sub>)] Where W is the relaxation parameter: OZWZI- relaxed Central - Difference Formulations For Velocity 0- 14 => U1,3 = 41,0+1-41,0-1 257  $V = \frac{\partial \Psi}{\partial x} = V_{i,j} = \frac{\Psi_{i+1,j} - \Psi_{i-1,j}}{2\Delta x}$ 

## Initial and Boundary Conditions Derivation



### **Program Listing**

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```
clear all;
clc;
N = [8 \ 16 \ 32];
Re = [10 100 400];
for l=1:length(N)
for r =1:length(Re)
%% Given
t_f = 3; % final time
dt = 0.01; % time step
u0 = 1; % velocity of lid
L x = 1; % x-length of cavity
L y = 1; % y-length of cavity
N x = N(1);  # of x-nodes
N y = N(1);  # of y-nodes
dx = L x/N x; % spatial-x step
dy = L y/N y; % spatial-y step
beta = dx/dy;
alpha = 1/(2*(1+beta^2));
w_PSOR = 0.9; % relaxation parameter for PSOR
ERROR TOL = 0.05; % error tolerance
Re r = Re(r); % Reynold's Number
%% Define Initial Conditions
u = zeros(N_x, N_y); % Define u velocity field
u(1, :) = 1; % initialize lid velocity
v = zeros(N_x,N_y); % Define v velocity field
% Initialize tridiagonal Matrix
tri x = zeros(N x, N y);
tri y = zeros(N_x, N_y);
% Initialize vorticity matrices
w x = zeros(N_x, N_y); % X-sweep
w y = zeros(N x, N y); % Y-sweep
w = zeros(N_x, N_y); % final vorticity matrix
% Initialize stream-function matrix
psi = zeros(N x, N y);
%% Boundary Conditions
w x(:,1) = 2*(psi(:,1)-psi(:,2))/dy^2;
w x(:,end) = 2*(psi(:,end)-psi(:,end-1))/dx^2;
w x(end,:) = 2*(psi(end,:)-psi(end-1,:))/dx^2;
w x(1,:) = 2*(psi(1,:)-psi(2,:))/dy^2 - 2*u0/dy;
w_y(:,1) = 2*(psi(:,1)-psi(:,2))/dy^2;
w_y(:,end) = 2*(psi(:,end)-psi(:,end-1))/dx^2;
w_y(end,:) = 2*(psi(end,:)-psi(end-1,:))/dx^2;
w_y(1,:) = 2*(psi(1,:)-psi(2,:))/dy^2 - 2*u0/dy;
w(:,1) = 2*(psi(:,1)-psi(:,2))/dy^2;
w(:,end) = 2*(psi(:,end)-psi(:,end-1))/dx^2;
w(end,:) = 2*(psi(end,:)-psi(end-1,:))/dx^2;
w(1,:) = 2*(psi(1,:)-psi(2,:))/dy^2 - 2*u0/dy;
```

```
% Define coefficents for tridiagonal matrix
d x = 1/Re r*dt/dx^2;
d v = 1/\text{Re r*dt/dv^2};
B x = 1 + d x;
B_y = 1 + d_y;
n = 1; % iteration level
t = 0; % current time
current error = 1;
while t < t_f%current_error > ERROR_TOL % loop until error is within the tolerance
   %% Boundary Conditions at next iteration level
    % Stream-Function
   psi(:,1, n+1) = psi(:,1, n);
   psi(1,:, n+1) = psi(1,:, n);
   psi(:,end, n+1) = psi(:,end, n);
   psi(end,:, n+1) = psi(end,:, n);
   % Velocity Fields
   u(1,:, n+1) = u(1,:,n);
   u(end,:, n+1) = u(end,:,n);
   u(:,1, n+1) = u(:,1,n);
   u(:,end, n+1) = u(:,end,n);
   v(1,:, n+1) = v(1,:,n);
   v(end,:, n+1) = v(end,:,n);
   v(:,1, n+1) = v(:,1,n);
   v(:,end, n+1) = v(:,end,n);
    % Vorticity Matrices
   w_x(:,1,n+1) = 2*(psi(:,1,n+1)-psi(:,2,n+1))/dy^2;
    w x(:,end,n+1) = 2*(psi(:,end,n+1)-psi(:,end-1,n+1))/dx^2;
    w_x(end,:,n+1) = 2*(psi(end,:,n+1)-psi(end-1,:,n+1))/dx^2;
    w x(1, :, n+1) = 2*(psi(1, :, n+1) - psi(2, :, n+1))/dy^2 - 2*u0/dy;
    w y(:,1,n+1) = 2*(psi(:,1,n+1)-psi(:,2,n+1))/dy^2;
    w_y(:,end,n+1) = 2*(psi(:,end,n+1)-psi(:,end-1,n+1))/dx^2;
    w y(end,:,n+1) = 2*(psi(end,:,n+1)-psi(end-1,:,n+1))/dx^2;
   w_y(1,:,n+1) = 2*(psi(1,:,n+1)-psi(2,:,n+1))/dy^2 - 2*u0/dy;
   w(:,1,n+1) = 2*(psi(:,1,n+1)-psi(:,2,n+1))/dy^2;
   w(:,end,n+1) = 2*(psi(:,end,n+1)-psi(:,end-1,n+1))/dx^2;
    w(end,:,n+1) = 2*(psi(end,:,n+1)-psi(end-1,:,n+1))/dx^2;
   w(1,:,n+1) = 2*(psi(1,:,n+1)-psi(2,:,n+1))/dy^2 - 2*u0/dy;
    %% Solve Vorticity-Transport Equation by ADI Method
    % 1st define tridiagonal matrices' elements
    for i = 1:N y
        for j = 1:N x
```

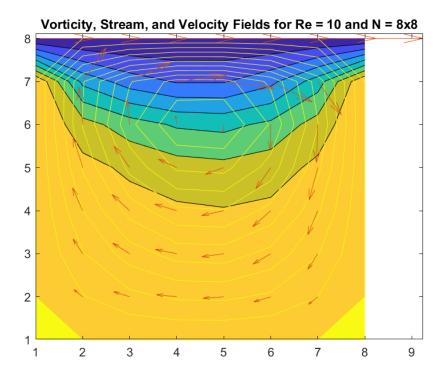
```
c_x(i,j) = u(i,j,n) * dt/dx;
            A_x(i,j) = -1/2*(1/2*c_x(i,j) + d_x);
            C x(i,j) = 1/2*(1/2*c x(i,j) - d x);
            c y(i,j) = v(i,j,n) * dt/dy;
            A_y(i,j) = -1/2*(1/2*c_y(i,j) + d_y);
            C_y(i,j) = 1/2*(1/2*c_y(i,j) - d_y);
            if i == j + 1 % Lower Diagonal
                tri_x(i,j) = A_x(i,j);
                tri y(i,j) = A y(i,j);
            elseif i == j % Main Diagonal
                tri x(i,j) = B x;
                tri_y(i,j) = B_y;
            elseif i == j - 1 % Upper Diagonal
                tri x(i,j) = C x(i,j);
                tri y(i,j) = C y(i,j);
            end
        end
    end
    % Perform X-SWEEP
    for i = 2:N_y-1 % Iterate bottom to top
        D x = [];
        for j = 2:N x-1 % Iterate left to right
            % initialize D matrix of "Ax = D"
            if j == 2
                D_ij = (c_y(i,j)/2+d_y)/2 * w(i,j-1,n) + (1-d_y)*w(i,j,n) + (-c_y(i, ∠
j)/2+d_y)/2*w(i,j+1,n) - A_x(i,j)*w(i,j-1,n);
            elseif j == N_x-1
                D ij = (c y(i,j)/2+d y)/2 * w(i,j-1,n) + (1-d y)*w(i,j,n) + (-c y(i, ⊮
j)/2+d y)/2*w(i,j+1,n) - C x(i,j)*w(i,j+1,n);
            else
                D_ij = (c_y(i,j)/2+d_y)/2 * w(i,j-1,n) + (1-d_y)*w(i,j,n) + (-c_y(i, ∠
j)/2+d_y)/2*w(i,j+1,n);
            end
            D x = [D x D ij];
        end
        % Solve for vorticity at ith row using Matlab '/' matrix operator
        w_i_x = D_x/tri_x(2:end-1, 2:end-1);
        w x(i, 2:end-1, n+1) = w i x;
    end
    % Y-SWEEP
    % 1st define tridiagonal matrices' elements
   % Perform Y-SWEEP
   for j= 2:N_x-1 % Iterate left to right
        D y = [];
        for i = 2:N_y-1 % Iterate bottom to top
            % initialize D matrix of "Ax = D"
           if i == 2
                D_{ij} = (c_x(i,j)/2+d_x)/2 * w_x(i-1,j,n) + (1-d_x)*w_x(i,j,n) + (-c_x \kappa)
(i,j)/2+d_x)/2*w_x(i+1,j,n) - A_y(i,j)*w_x(i-1,j,n+1);
```

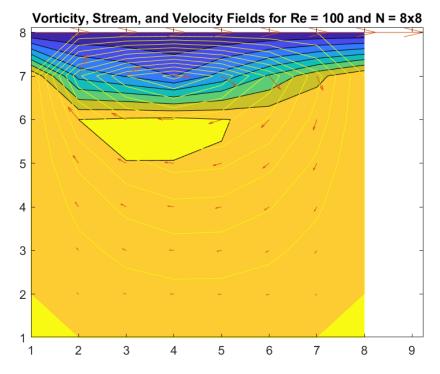
```
elseif i == N y-1
                D_ij = (c_x(i,j)/2+d_x)/2 * w_x(i-1,j,n) + (1-d_x)*w_x(i,j,n) + (-c_x ⊮
(i,j)/2+d_x)/2*w_x(i+1,j,n) - C_y(i,j)*w_x(i+1,j,n+1);
            else
                D_ij = (c_x(i,j)/2+d_x)/2 * w_x(i-1,j,n) + (1-d_x)*w_x(i,j,n) + (-c_x ∠
(i,j)/2+d x)/2*w x(i+1,j,n);
            end
            D y = [D y D ij];
        end
        % Solve for vorticity at jth column using Matlab '/' matrix operator
        w j y = D y/tri y(2:end-1, 2:end-1);
        w y(2:end-1, j, n+1) = w j y;
        w = w_y;
    end
    %% Solve Stream Function by PSOR
    PSOR error = 1; % initialize current PSOR error
    count = n;
    while PSOR error > ERROR TOL % iterate until PSOR error is within the tolerance
        psi_old = psi(:,:,end-1);
        for i = 2:N y-1
            for j = 2:N x-1
                psi(i,j,n+1) = (1-w_PSOR)*psi(i,j,n) + w_PSOR*alpha*(w(i,j,n+1)*dx^2+ #
psi(i+1,j,n) + psi(i-1,j,n+1)+beta^2*(psi(i,j+1,n)+psi(i,j-1,n+1)));
           end
        end
        psi old = psi(:,:,end-1);
        PSOR error = max(max(abs(psi(:,:,end) - psi old)));
    end
    n = count;
    %% Initialize new velocity fields
   for i = 2:N y-1
        for j = 2:N \times -1
            u(i, j, n+1) = (psi(i, j+1, n) - psi(i, j-1, n)) / (2*dy);
            v(i,j,n+1) = -(psi(i+1,j,n)-psi(i-1,j,n))/(2*dx);
        end
    end
    %% Update Counters and Error to Check for Convergence
    current_error = max(max(abs(w_y(2:end-1,2:end-1,n+1) - w_y(2:end-1,2:end-1,n))));
    n = n + 1; % increment iteration level
    t = t + dt; % increment time
end
w_flipped = flipud(w(:,:,end));
psi flipped = flipud(psi(:,:,end));
u flipped = flipud(u(:,:,end));
v flipped = flipud(v(:,:,end));
%% Plots
```

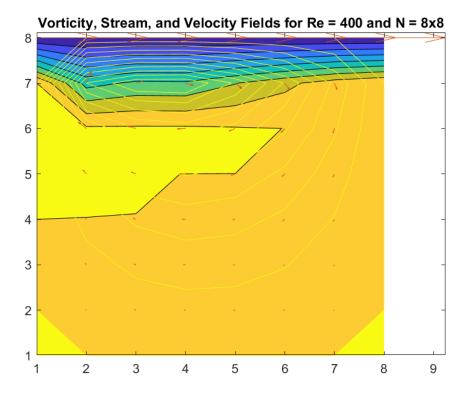
```
Re_str = num2str(Re(r));
```

```
N_str = num2str(N(1));
figure(3*(1-1)+r) % Vorticity Plot
contourf(w_flipped)
hold on
%title(['Vorticity for Re = ', Re_str, ' and N = ', N_str, 'x', N_str]);
%figure(3*(1-1)+r+1) % Stream-function Plot
contour(psi_flipped)
hold on
%title(['Stream Function for Re = ', Re_str, ' and N = ', N_str, 'x', N_str]);
%figure(3*(1-1)+r+2) % Velocity-field Plot
quiver(u_flipped(2:end-1,2:end-1), v_flipped(2:end-1,2:end-1), 1)
title(['Vorticity, Stream, and Velocity Fields for Re = ', Re_str, ' and N = ', K
N_str, 'x', N_str]);
end
end
```

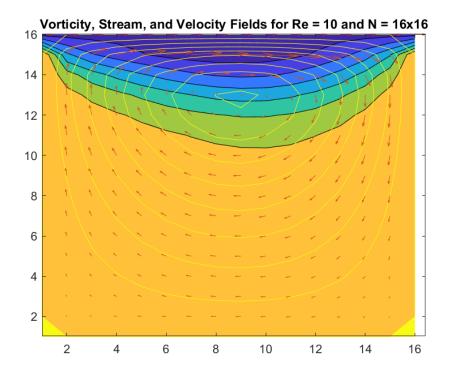
## Program Results 8 x 8 Grid Results

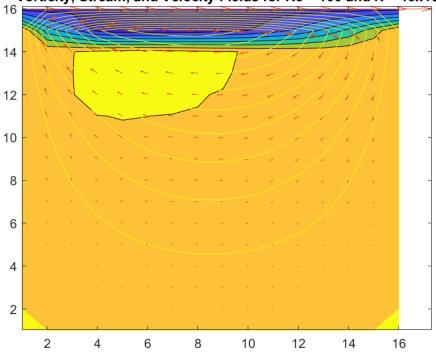




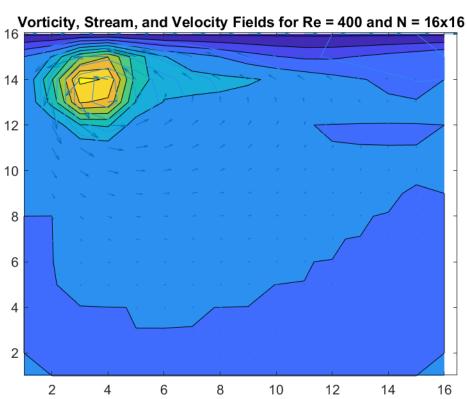


#### 16 x 16 Grid Results

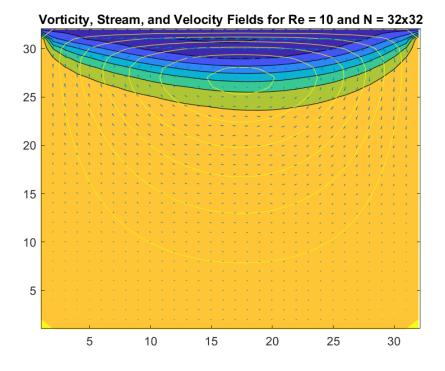


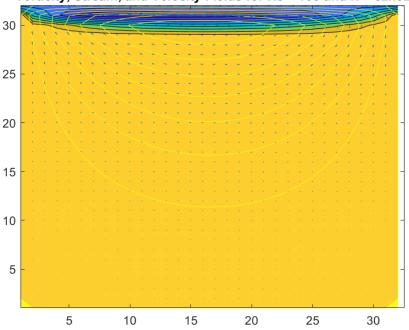


Vorticity, Stream, and Velocity Fields for Re = 100 and N = 16x16



#### 32 x 32 Grid Results





Vorticity, Stream, and Velocity Fields for Re = 100 and N = 32x32

## Discussion

In each figure, there are separation points (yellow portions of the plot) at the bottom corners of the cavity. For Reynolds numbers of 100 there is additional separation occurring off the left wall and below the location of maximum vorticity, and for Reynolds numbers of 400 there seems to be separation at the locations of high vorticity.

The nature of the results change depending on the number of nodes being solved, which is a sign that the computations were improperly implemented into MATLAB. Rather than seeing entirely different results altogether for higher node-counts, we should expect to see the same results shown in higher resolution.